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Transmitted herewith for filing under 35 U.S.C. 111 and 37 C.F.R. 1.53 is the patent application of:

Ronald A. Guidotti, et al.

For: **Energy Storage and Conversion Devices Using Thermal Sprayed Electrodes**

Enclosed are:

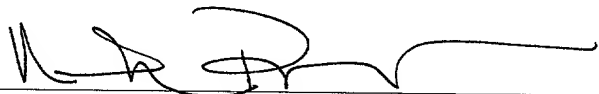
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Dated: **November 2, 1999**

  
Signature

Leah M. Reimer  
Registration No.: 39,341  
Cantor Colburn LLP  
88 Day Hill Road  
Windsor, CT 06095  
(860) 688-4470

cc:

## ENERGY STORAGE AND CONVERSION DEVICES USING THERMAL SPRAYED ELECTRODES

### Background of the Invention

#### 1. Field of the Invention.

This invention relates to energy storage and conversion devices, and in particular, to energy conversion and storage devices using thin film oxide and non-oxide electrodes manufactured by thermal spray.

#### 2. Description of the Related Art

Energy storage devices, such as batteries and supercapacitors, and energy conversion devices, such as fuel cells and thermoelectrics, both require electrodes comprising an active material for the energy storage, conversion, and/or release processes. Each year, billions of dollars are spent on both primary and rechargeable batteries for use in applications ranging from small batteries for portable electronics and communications equipment, to larger batteries used for automobiles and uninterruptible power supplies (UPS).

The LiSi/FeS<sub>2</sub> couple is the primary power source used for thermally activated batteries ("thermal batteries") for some nuclear weapons and missiles, as described in U.S. Patent Nos. 4,119,769, 4,840,859, and 4,675,257, which are incorporated by reference herein. These batteries are designed to function only when the electrolyte phase becomes molten. Until the internal pyrotechnic heat source is ignited, the batteries are inert and have an almost

unlimited shelf life. Common electrolytes used for these applications include the LiCl-KCl eutectic that melts at 352 °C and the all-lithium LiCl-LiBr-LiF minimum-melting electrolyte that melts at 436 °C. The cathode, separator, and anodes for thermally activated batteries are prepared by cold pressing of powders in dies. The separator contains enough MgO (typically, 35 weight. %) to act as an immobilization agent for the electrolyte once the battery has been activated and the electrolyte melts. The catholyte contains 25% or more of separator material and, in many cases, 1.5% Li<sub>2</sub>O to act as a lithiation agent to mitigate voltage transients caused by electroactive iron impurities. The anode contains 20-25% electrolyte to aid in pelletizing and to improve the electrochemical performance by increasing the ionic conductivity. Each cell in a bipolar thermal-battery stack contains pellets of anode, separator, cathode, and pyrotechnic source (typically, Fe/KClO<sub>4</sub> blends) and 304 stainless steel current collectors between the anode and the heat pellet and between the heat pellet and cathode of the adjacent cell. These also serve as thermal buffers to moderate the heat input to the active cell components. This is important for the FeS<sub>2</sub> (pyrite) cathode, in that FeS<sub>2</sub> becomes thermally unstable above 550 °C, decomposing according to equation 1:



Under these conditions, the fugitive sulfur vapor can react with the LiSi anode to generate enough heat to cause a thermal-runaway condition, where the battery self-destructs.

The need to press catholyte powders such as FeS<sub>2</sub> into thin films or pellets for use in thermal batteries increases production costs because of the high labor costs associated with processing of the material (e.g., blending, pelletizing, and quality control checks for weight and thickness). While the current technology of using cold-pressed pellets is suitable for its

intended purposes, it has a number of intrinsic limitations. The thinnest pellets that can be fabricated with reasonable yields are in the range from 0.010 to 0.012 inches in thickness. For many applications this results is far greater capacity than is actually needed. The use of a graphite-paper substrate as a reinforcing agent greatly helps with the cathode pellet, but is not an option with the separator and anode pellets, however. The use of excess material increases the length and mass of the thermal battery unnecessarily. Pressing of large pellets becomes increasingly more difficult as the diameter of the pellet is increased from 1 inch to 5 inches. The necessary pressure for compaction of pellets increases rapidly as the square of the area of the pellet, so that presses with capacities of 500 tons or more are needed for the larger pellets. Such large presses are very expensive.

Thin films, and thin film electrodes in particular have been fabricated by other techniques, including spray pyrolysis and chemical vapor deposition (CVD). Spray pyrolysis has been used to fabricate electrodes comprising  $\text{LiCoO}_2$ ,  $\text{LiMn}_2\text{O}_4$ , and yttria stabilized zirconia (YSZ). CVD has been used to fabricate electrodes comprising  $\text{MoS}_2$  (by conventional CVD),  $\text{ZrO}_2\text{-TiO}_2\text{-Y}_2\text{O}_3$  (by laser CVD, wherein the laser is the heat source of the substrate and reaction activator), and  $\text{TiS}_2$  (by plasma CVD). Thin film electrodes have also been prepared by sol-gel methods ( $\text{CeO}_2\text{-TiO}_2$  electrodes), electrochemical method (amorphous  $\text{MnO}_2$  electrodes), and molecular beam deposition ( $\gamma\text{-In}_2\text{Se}_3$ ). An approach to fabrication of electrodes by thermal spray has been reported by R. Henne (Institute für Technische Thermodynamik, Stuttgart, Germany) for at least one energy conversion device, a solid oxide fuel cell, wherein yttria-stabilized zirconia (YSZ) and porosity-graded perovskite deposited by DC are thermal sprayed to fabricate multilayer structures. R. Zatorski of Sulzer-

Metco has also reported production of battery electrodes by thermal spray techniques.

However, the above reports are directed to thermally stable materials which do not decompose at the high temperatures generally required for thermal spray.

Synthesis of thin films of pyrite in particular has previously been investigated. G.

5 Pimenta et al. have produced pyrite using  $H_2S$ -reactive iron. Pyrite and pyrite films have also been prepared by chemical vapor transportation, sulfurization of iron oxides, electrodeposition of iron films, argon and reactive sputtering, screen printing processes, and chemical vapor deposition. Conventional and fine pyrite (micron-sized) is also produced in aqueous solution. Nonetheless, despite the variety of methodologies available for the production of thin films,  
10 there remains a need for energy storage and energy conversion devices with effective pyrite couples that are efficiently and easily produced.

#### Summary of the Invention

The above-discussed and other drawbacks and deficiencies of the prior art are  
15 overcome or alleviated by the energy storage devices and energy conversion devices of the present invention, having thin cathodes comprising pyrite or other active materials produced by thermal spray techniques. In a particularly advantageous feature, the active materials are metal sulfides which ordinarily decompose or are unavailable at the high temperatures used during thermal spray processes, such as such as pyrite,  $CoS_2$ ,  $WS_2$ ,  $MoS_2$ ,  $NiS_2$ , and the like.  
20 The active material feedstocks for thermal spray of these materials are readily available, for example by chemical synthesis in aqueous solution at low temperature ( $<90^\circ C$ ). The active material feedstock may furthermore comprise microstructured or nanostructured materials,

which after thermal spray results in electrodes having microstructured or nanostructured active materials, respectively.

The above-discussed and other features and advantages of the present invention will be appreciated and understood by those skilled in the art from the following detailed description and drawings.

#### Brief Description of the Drawings

FIGURE 1 is a graph showing discharge of a conventional pelletized  $\text{LiSi/FeS}_2$  single cell at 500 °C at 125 mA/cm<sup>2</sup> background load (1-second pulses of 250 mA/cm<sup>2</sup> were applied every 60 seconds).

FIG. 2 is a photomicrograph of a cross-sectioned sample of early deposit identified by x-ray diffraction analysis as troilite.

FIG. 3 is a graph showing discharge of a single cell made with plasma-sprayed pyrite containing troilite.

FIG. 4 is a graph showing discharge of pyrite plasma-sprayed under partial pressure of sulfur.

FIG. 5 is a graph showing the comparison of discharge behavior of cells for various pyrite sources.

FIG. 6 is a graph showing cell resistances of single cells discharged at 500 °C for various sources of pyrite.

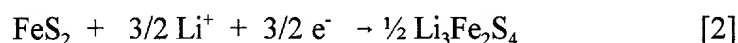
### Detailed Description of the Preferred Embodiments

In accordance with the present invention, energy storage devices and energy conversion devices comprising thin electrodes may be produced by thermal spray techniques. Thermal spray, and in particular plasma spray techniques, are advantageous in that the morphology and phase of the coating can be controlled, as well as the deposit thickness of the coating. Thus, very thin films (e.g., as thin as 1 micron) are available, up to reasonably thick films (e.g., up to 1, and even up to 10 millimeters). Films in the range of about 1 to about 200 microns are preferred, and film in the range of about 0.2 to 4.5 mils (5 to 114 microns) have been produced, and are particularly preferred, as allowing significant increases in specific energy and energy density.

Thermal spray methods involve heating feedstock particles to a molten or plastic state, and propelling the heated particles onto a substrate to form a coating. Methods and apparatus for thermal spray are well known, being described, for example, in U.S. Patent Nos. 4,869,936, 5,080,056, 5,198,308, 5,271,967, 5,312,653, and 5,328,763, which are incorporated by reference herein. However, a number of potential active materials for electrodes have not been previously accessible by thermal spray, because they decompose at the temperatures required to transform the feedstock particles to a molten or plastic state (e.g., pyrite), or are converted to forms which are unsuitable for use as battery components. In a particularly advantageous feature of this invention, the active materials are metal sulfides which ordinarily decompose or are unavailable at the high temperatures used during thermal spray processes, such as pyrite,  $\text{CoS}_2$ ,  $\text{WS}_2$ ,  $\text{NiS}_2$ ,  $\text{MoS}_2$ , and the like. The metal sulfides are

protected from decomposition or other undesirable transformation by the presence of a thermally protective barrier coating comprising elemental sulfur.

Pyrite in particular is useful in thermal batteries. The LiSi/FeS<sub>2</sub> couple of thermally activated batteries comprises FeS<sub>2</sub> (pyrite) as a cathode. The electrochemical performance of a standard LiSi/FeS<sub>2</sub> cell made with conventional pellets cold pressed from powders is shown in FIG. 1, along with the corresponding cell resistance, wherein the resistance of the cell was calculated from the voltage drop during the pulses and included non-ohmic as well as IR contributions. The upper plateau voltage is represented by equation 2:



The theoretical capacity of the FeS<sub>2</sub> for this reaction is 1,206 coulomb/g.

The first voltage transition starting near 480 s is due to discharge of Li<sub>3</sub>Fe<sub>2</sub>S<sub>4</sub> to a complex mixture of lower sulfides of iron, Li<sub>2-x</sub>Fe<sub>1-x</sub>S<sub>2</sub> + Fe<sub>1-x</sub>S, where x is about 0.2. The much larger voltage transition near 1,000 s is related to formation of Li<sub>2</sub>FeS<sub>2</sub> (Li<sub>2</sub>S + FeS). These transformations were verified to be cathode related in tests that incorporated a Ag/AgCl reference electrode. The anode phase transformation that occurs would not take place until well after 1,200 s. With the masses of anode and cathode used in this work, the cells were cathode limited. The increase in resistance that occurs at the voltage transitions as shown in FIG. 1 is related to the change in resistance of the discharge phases. The resistance of Li<sub>3</sub>Fe<sub>2</sub>S<sub>4</sub> is much greater than that of FeS<sub>2</sub> and Li<sub>2</sub>FeS<sub>2</sub>, which explains the shape of the curve.

Two techniques for thermal spray of pyrite cathodes were examined. The first used high-velocity oxygen flame (HVOF), wherein the feedstock was directly injected into a



hydrogen-oxygen flame that rapidly expands at the nozzle exit before impinging onto the collection substrate of 0.010 inch thick 304 stainless steel. Initial results with the HVOF system were not successful, in that it was not possible to provide a sufficiently reducing atmosphere to prevent oxidation of  $\text{FeS}_2$ . XRD analysis showed that the deposits consisted primarily of  $\text{Fe}_2\text{O}_3$  with minor amounts of pyrite, pyrrhotite ( $\text{Fe}_{1-x}\text{S}$ ), and greigite ( $\text{Fe}_3\text{S}_4$ ). The lower-sulfide phases are undesirable due to their much lower emf (about 1.25 V vs. LiSi) relative to that of pyrite (about 2.0 V at 500 °C).

A second technique used dc-arc plasma spray under an argon cover (250 SCFH) with arc currents of between 200 A and 300 A. To minimize potential oxidation of the pyrite during spraying, a protective enclosure was constructed and a cover gas of argon was used. In later tests, elemental sulfur was added to the pyrite feedstock to aid in processing and to suppress  $\text{FeS}_2$  decomposition. Initial test results showed reasonably good adhesion of the deposit to the substrate. A photomicrograph of a cross-sectioned sample is shown in FIG. 2. The deposited material was relatively dense. X-ray diffraction (XRD) analysis showed the primary phase to be troilite ( $\text{Fe}_7\text{S}_8$ ), rather than pyrite.

The discharge trace for a representative sample of this material (0.122 g, 0.0012 inches thick) is shown in FIG. 3. The elevated voltage during open circuit at the start of the test was due to oxidized Fe species and possibly sulfur. However, there was no upper-voltage plateau present when the cell was placed under load. Only the lower-voltage plateau for the FeS-containing phase was evident. This is consistent with the XRD data for the presence of troilite. The resistance of the cell was comparable to that of the cell with natural pyrite, even

though the resistivity of the troilite is higher than that of pyrite. The improved contact of the deposit with the substrate may be responsible for this.

It was recognized that pyrite is thermally unstable, decomposing to FeS at about 550 °C. The flame temperature of plasmas is thus much hotter than the decomposition temperature of pyrite. In order to prevent decomposition, several tests were conducted in which a protective barrier coating, elemental sulfur, was blended with the pyrite and then ball milled before injection into the plasma. Sulfur has a melting point at 120 °C and boiling point at 440 °C, such that both its melting point and boiling point are below the decomposition temperature of pyrite. Without being bound by theory, according to LeChatelier's Principle, the thermal decomposition of pyrite (Eq. 1) should be driven to the left in the presence of sulfur vapor. Since the sulfur additive has formed S<sub>2</sub> gas around the solid pyrite particles above 440 °C, the additional sulfur gas partial pressure favors the reversible reaction, i.e., formation of pyrite. Consequently, the decomposition is further prevented. Alternatively, or in addition, the presence of sulfur may provide a thermally protective shield between the particles and the plasma flame. Sulfur is not a good heat conductor, and the sulfur coating may consume a large amount of energy while the solid state sulfur transforms to liquid and gas phase. A similar strategy may also be employed for thermal spray of certain other metal-based active materials, for example metal selenides and metal tellurides. Metal selenides, for example metal diselenides are accordingly coated with an effective quantity of selenium prior to thermal spray, and metal tellurides, for example metal ditellurides are coated with an effective quantity of tellurium.

In addition to elemental sulfur, selenium, or tellurium, other organic and inorganic sources of elemental sulfur, selenium, or tellurium may also be used. A combination of a

source of elemental sulfur, selenium, or tellurium with other protective barrier coating materials may also be used, such alternative materials including inert, low heat conductive materials such as cornstarch or PVA. The total effective quantity of the protective barrier coating material may vary, depending on factors such as cost, spray temperature, and effectiveness. For example, about 1 to about 30% by weight of sulfur (relative to weight of pyrite) is generally effective for use with dc-plasma arc, and about 5 to about 20% by weight is preferred.

XRD examination of a number of deposits prepared using pyrite/sulfur feedstocks showed the major phase to be pyrite, with a minor amount of pyrrhotite. The results of single-cell tests with this material are summarized in FIG. 4 for a deposit mass of 0.1983 g (0.002 inches thick). The initial voltage transient was still evident from electroactive impurities with a higher emf than  $\text{FeS}_2$ , but a well-defined upper plateau was now evident which corroborates the XRD data. The results of these tests indicate the advantage of maintaining a substantial sulfur vapor pressure during plasma spraying of pyrite in order to obtain the desired stoichiometry.

The resistance of the cell was initially higher but dropped quickly to that of the standard cell as discharge progressed. The initial higher resistance may be due to poor wetting of the sample at the start of discharge. The dense substrate does not allow immediate access to the rear of the sample until porosity is induced during discharge. The resistance of the cell paralleled that observed for the cell with natural pyrite, except that cell resistance did not change as dramatically at the phase transitions, especially at the end of discharge. The much higher resistance in the former case may reflect a reduction in particle-particle contact during discharge which is absent in the case of the monolithic plasma-sprayed deposit which

has improved interfacial contact with the stainless steel current collector. The capacities of the plasma-sprayed materials deposited under sulfur vapor to a cutoff voltage of 1.25 V ranged from 2,760 to 2,938 coulombs/g, which was comparable to that for the conventional cathode of 2,740 coulomb/g.

5           The data from FIGS. 1 and 4 are normalized on a sample mass basis and are presented in FIG. 5 for the steady-state voltage, after correcting for the open-circuit time. The voltage for the pyrite plasma sprayed with sulfur tracks that of the natural pyrite quite well and is actually slightly higher after the major voltage transition. This indicates lower polarization for this material. Comparable data are presented in FIG. 6 for the cell resistance. The resistance hump normally seen with cells with cold-pressed cathodes is conspicuously absent for the plasma-sprayed materials.

10           It has furthermore been unexpectedly discovered that with the incorporation of sulfur into the pyrite feedstock, a sufficiently high partial pressure of sulfur is maintained which represses the thermal decomposition of pyrite. Thin (0.2 - 4.5 mils) films of predominantly pyrite are obtained that show good electrochemical behavior at 500 °C in single-cell tests. Cell resistances were comparable during initial discharge and slightly lower deeper into discharge than those of the standard cell with pressed-powder cathodes. Use of thermal spray also results in strong adhesion of the pyrite, which leads to reduced interfacial resistance between the current collector and the cathode. Lower impedance would result in a higher power output. A monolithic pyrite cathode also reduces the interparticle resistance associated with pressed compacts, which could further increase power capability.

20           The active material feedstock may furthermore comprise a microstructured or nanostructured material, which after thermal spray results in electrodes with microstructured

or nanostructured active material, respectively. As used herein, "microstructured" materials refers to materials having a grain size on the order of about 0.1 to about 500 micrometers (microns), and "nanostructured" materials refers to materials having a grain size on the order of about 1 to about 100 nanometers (where 1 nm = 10 angstroms). Nanostructured materials are thus characterized by having a high fraction of the materials' atoms residing at grain or particle boundaries. For example, with a grain size in the five nanometer range, about one-half of the atoms in a nanocrystalline or a nanophase solid reside at grain or particle interfaces. Rapid interaction between the active materials and its surroundings are possible because of high surface area of the nanostructured materials. Therefore, the materials could sustain high current charging and discharging conditions. Thermal spray of nanostructured feedstocks to produce nanostructured coatings is disclosed in allowed U.S. patent application Serial No. 09/019061, filed February 5, 1998, entitled "Nanostructured Feeds for Thermal Spray Systems, Method of Manufacture, and Coatings Formed Therefrom," which is a continuation of U.S. patent application Serial No. 08/558,466 filed November 13, 1995, which is incorporated herein by reference. Active material feedstocks comprising larger grain sizes are also within the scope of the present invention.

Thermal spray methods are thus particularly effective in the production of electrodes for energy storage and conversion devices, for example a cathode electrode incorporated into a primary electrochemical cell, or the anode and/or the cathode of a secondary electrochemical cell. Such electrodes may be readily and economically manufactured by thermal spray of a suitable substrate, for example stainless steel, titanium or aluminum, followed by punching or cutting the substrate into suitable shapes. The electrodes thus comprise active materials which

decompose or are otherwise unavailable at temperatures required for thermal spray techniques.

The invention is further illustrated by the following non-limiting examples.

5

## EXAMPLES

### A. Reprocessing of Pyrite

About 20 grams of sulfur powder is mixed with 200 grams of pyrite powder and ball milled in a ceramic jar for 24 hours. The uniformly mixed powder is then placed in a vacuum oven and dried at 150 °C under vacuum for 12 hours. The surface moisture of pyrite is thereby removed and the surface of the pyrite coated by sulfur due to its low melting point (about 120 °C). The treated powder has much better flowability, and due to high dihedral angle between sulfur and water, the treated powder was not required to be store under vacuum.

10

### B. Apparatus

In general, a plasma gun is connected with a robot which has six dimension movement, and the workpiece is fixed on the sample stage. An alternative apparatus consists of a stainless steel box having a front cover accommodating a fixed plasma gun, a nitrogen gas inlet, and a robot connected to a sample holder. With this apparatus, the sample moves instead of the plasma gun, which is sealed with rubber between the front cover and the stainless steel box. With this apparatus, the oxygen content inside the chamber could be reduced to less than 5%.

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### C. Thermal Spray of Conventional (Micron and Greater-Sized) Pyrite Feedstock

Prior to thermal spray, the inert gas chamber is purged with nitrogen gas for 10 minutes. With the treated powder, coatings were produced using a Metco 9MB plasma spray system. At about 150 Ampere and 70 Volts, with 250 SCFH argon flow and 4 lb/hr feeding rate, electrodes were sprayed at conditions 3c and 5b on 1.25 inch diameter 0.006 inch thick grit blasted stainless steel disks. At both 200 and 300 Amp 250 SCFH argon conditions, the coating adhered well to the substrate, and was not fragile during handling. Also, little curling occurred indicating low stresses and the potential to spray much thicker layers.

The adjustable parameters of the plasma gun include arc current and argon flow rate. By reducing the arc current, increasing the argon flow rate and carrier gas rate, the flame temperature could be reduced further. However, the over-cooled flame could not melt the surface of particles and the quality of coating would thus deteriorate. The optimized condition is 180A, with 250 SCFH argon flow. The experiments have been carried out in the inert gas chamber with the best plasma spray conditions. The results show no evidence of iron oxide present in the deposited films. The x-ray pattern also indicates that there is more iron sulfide left in the coating compared to the one without the protection of an inert gas chamber.

X-ray data of the films resulting from spray of the reprocessed pyrite show that without sulfur additive the thin film comprises  $\text{FeS}$ ,  $\text{FeS}_x$  (where  $x < 2$ ),  $\text{Fe}_2\text{O}_3$ ,  $\text{Fe}_3\text{O}_4$  and other undesired phases. With sulfur additive, the primary phase of the thin film (>95 %) is  $\text{FeS}_2$ .

In later experiments, reprocessed pyrite was thermal sprayed onto stainless steel coupons in air, i.e., without use of the inert gas chamber, wherein the plasma gun is mounted on the robot and the sample on the specimen stripe. The XRD data for these samples resembled those for the deposited material, being predominantly pyrite.

D. Reprocessing of Nanostructured Pyrite.

Nanostructured pyrite is synthesized by aqueous solution method at low temperature (<90°C) in relatively short period (2-4 hours). Synthesized nanostructured FeS<sub>2</sub> has a particle size less than 100 nm. About 20 grams of sulfur powder was mixed with 200 grams of the nanostructured pyrite powder and ball milled in a ceramic jar for 24 hours. Thereafter, the uniformly mixed powder is placed in a vacuum oven, and dried at 150° C under vacuum for 12 hours. The treated powder then is dispersed in 10% PVA solution and the suspension is then spray dried at 200° C in accordance with U.S. Ser. No. 08/553,133 above. The particle size of reprocessed powder is in the range of 1-200 microns.

E. Thermal Spray of Pyrite Thin Film Electrode.

Dc-arc plasma spray under an argon cover (250 SCFH) was used, with arc currents of between 200 A and 300 A, using a Metco 9MB plasma spray system. Cornstarch was added to the FeS<sub>2</sub> as a fugitive flow enhancer. To minimize potential oxidation of the pyrite during spraying, a protective enclosure was constructed and a cover gas of argon was used. In later tests, elemental sulfur was added to the pyrite feedstock to aid in processing and to suppress FeS<sub>2</sub> decomposition.

F. Electrochemical Testing

The plasma-sprayed pyrite samples were fabricated into 1.25 inch diameter single cells with 44 w/o Li/Si anodes and separators based on 35% MgO and LiCl-KCl eutectic. The mass of active FeS<sub>2</sub> in each sample was determined to allow gravimetric efficiencies to be calculated. Cells were discharged galvanostatically between heated platens at 500 °C under



computer control in a glovebox under an atmosphere of high-purity argon. A steady-state current of 1 A ( $\sim 125 \text{ mA/cm}^2$ ) was used with a 1-second, 2 A ( $\sim 250 \text{ mA/cm}^2$ ) pulse applied every minute. This allowed the overall cell resistance to be calculated. The cells were discharged to a cutoff voltage of 0.5 V.

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While preferred embodiments have been shown and described, various modifications and substitutions may be made thereto without departing from the spirit and scope of the invention. Accordingly, it is to be understood that the present invention has been described by way of illustration and not limitation.

What is claimed is:

1. A method for the manufacture of an electrode for an energy storage and conversion device, comprising

providing a feedstock mixture comprising an effective quantity of a source of elemental sulfur and a metal sulfide, an effective quantity of a source of elemental selenium and a metal selenide, or an effective quantity of a source of elemental tellurium and a metal telluride; and

thermally spraying the feedstock mixture onto a substrate, to produce a film of the active material having a thickness in the range from about 1 to about 1000 microns.

2. The method of claim 1, wherein the feedstock mixture comprises a source of elemental sulfur and metal sulfide.

3. The method of claim 2, wherein the metal sulfide is  $\text{FeS}_2$ ,  $\text{CoS}_2$ ,  $\text{WS}_2$ ,  $\text{NiS}_2$ , or  $\text{MoS}_2$ .

4. The method of claim 3, wherein the metal sulfide is  $\text{FeS}_2$ .

5. The method of claim 1, wherein the feedstock mixture further comprises a second inert, thermally protective barrier coating.

6. The method of claim 1, wherein the feedstock mixture comprises elemental sulfur and  $\text{FeS}_2$ .

7. The method of claim 1, wherein thermal spraying is by dc-arc plasma spray.

8. The method of claim 1, wherein the films have a thickness in the range from about 5 to about 200 microns.

9. The method of claim 1, wherein the feedstock active material is microstructured.

10. The method of claim 1, wherein the feedstock active material is nanostructured.

11. A method for the manufacture of an electrode for an energy storage and conversion device, comprising

ball-milling an active material feedstock comprising a metal sulfide with from about 1 to about 30 % by weight of a source of elemental sulfur, a metal selenide with from about 1 to about 30 % by weight of a source of elemental selenium, or a metal telluride with from about 1 to about 30 % by weight of a source of elemental tellurium to provide a feedstock for thermal spray; and

thermally spraying the feedstock for thermal spray onto a substrate, to produce a film of active material having a thickness in the range from about 1 to about 1000 microns.

12. The method of claim 11, wherein the feedstock mixture comprises a source of elemental sulfur and metal sulfide.

13. The method of claim 12, wherein the metal sulfide is  $\text{FeS}_2$ ,  $\text{CoS}_2$ ,  $\text{WS}_2$ ,  $\text{NiS}_2$ , or  $\text{MoS}_2$ .

14. The method of claim 13, wherein the metal sulfide is  $\text{FeS}_2$ .

15. The method of claim 11, wherein the feedstock mixture further comprises a second inert, thermally protective barrier coating.

16. The method of claim 11, wherein the feedstock mixture comprises elemental sulfur and  $\text{FeS}_2$ .

17. The method of claim 11, wherein thermal spraying is by dc-arc plasma spray.

18. The method of claim 11, wherein the film has a thickness in the range from about 5 to about 200 microns.

19. The method of claim 11, wherein the feedstock active material is microstructured.

20. The method of claim 11, wherein the feedstock active material is nanostructured.

21. A electrode for an energy storage and conversion device, comprising

a substrate; and

a layer of an active material comprising a metal sulfide, metal selenide, or metal

telluride, and having a thickness in the range from about 1 to about 1000 microns deposited

on the substrate, wherein the active material decomposes or transforms to a material

unsuitable for use in an electrode at thermal spray temperatures.

22. The electrode of claim 21, wherein the layer of active material has a thickness

in the range from about 1 to about 200 microns.

23. The electrode of claim 21, wherein the layer of active material has a thickness

in the range from about 5 to about 114 microns.

24. The electrode of claim 21, wherein the active material is a metal sulfide.

25. The method of claim 21, wherein the active material is  $\text{FeS}_2$ ,  $\text{CoS}_2$ ,  $\text{WS}_2$ ,  $\text{NiS}_2$ ,

or  $\text{MoS}_2$ .

26. The electrode of claim 21, wherein the active material is  $\text{FeS}_2$ .

27. The method of claim 21, wherein the active material is microstructured.

28. The method of claim 21, wherein the active material is nanostructured.

29. A method for the manufacture of an electrode, comprising  
providing a feedstock mixture comprising an effective quantity of a protective barrier  
coating comprising a source of elemental sulfur and pyrite; and  
thermally spraying the feedstock mixture onto a substrate, to produce a film of pyrite  
active material having a thickness in the range from about 1 to about 1000 microns.

30. The method of claim 29, wherein the feedstock mixture comprises from about  
1 to about 30% by weight of elemental sulfur.

31. The method of claim 29, wherein thermal spraying is by dc-arc plasma spray.

32. The method of claim 29, wherein the film has a thickness in the range from  
about 1 to about 200 microns.

33. The method of claim 29, wherein the film has a thickness in the range from  
about 5 to about 114 microns.

34. A method for the manufacture of a cathode, comprising  
ball-milling pyrite with from about 1 to about 30 % by weight of elemental sulfur, to  
provide a feedstock comprising sulfur and pyrite; and  
thermally spraying the feedstock solution onto a substrate, to produce a film of pyrite  
active material having a thickness in the range from about 1 to about 200 microns.

35. The method of claim 34, wherein thermal spraying is by dc-arc plasma spray.

36. The method of claim 34, wherein the film has a thickness in the range from about 5 to about 114 microns.

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37. A cathode, comprising

a substrate; and

a layer of pyrite active material deposited on the substrate, wherein the layer of pyrite has a thickness in the range from about 1 to about 1000 microns.

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38. The method of claim 37, wherein thermal spraying is by dc-arc plasma spray.

39. The method of claim 37, wherein the layer has a thickness in the range from about 1 to about 200 microns.

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40. The method of claim 37, wherein the layer has a thickness in the range from about 5 to about 114 microns.

## Abstract

Thin electrodes produced by thermal spray techniques are presented, wherein the thermal spray feedstock comprises an active material and a protective barrier coating. In a particularly advantageous feature, the active material feedstock is a metal sulfide, metal selenide, or metal telluride which ordinarily decomposes at thermal spray temperatures or which transforms to a material unsuitable for use as an electrode at thermal spray temperatures. The electrodes find particular utility in thermal batteries.



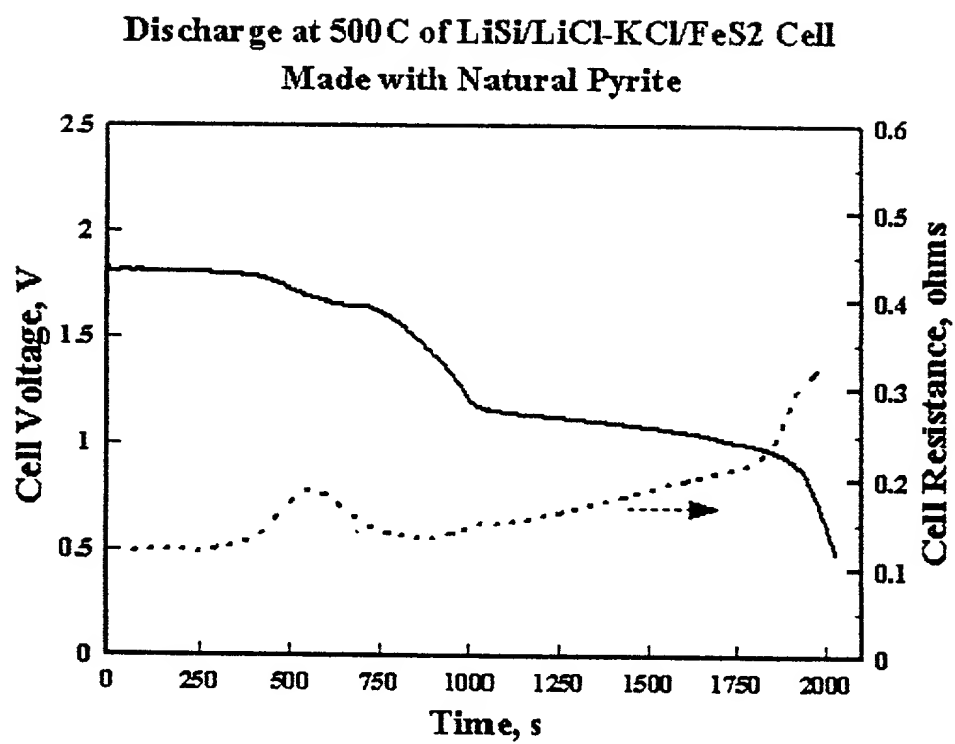


Figure 1.

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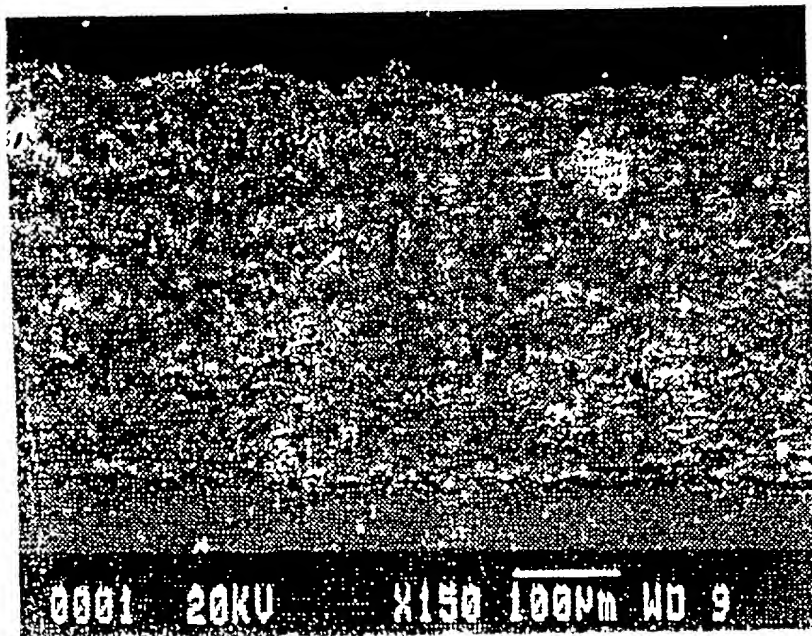


Fig 2

Discharge at 500C of LiSi/LiCl-KCl/FeS<sub>2</sub> Cell  
Made with Pyrite Plasma Sprayed without Sulfur

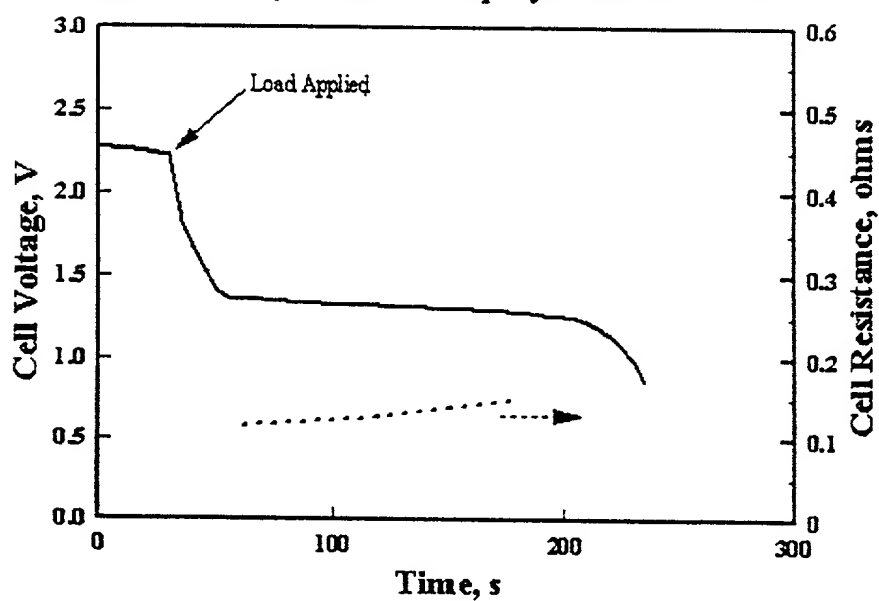


Figure 3.

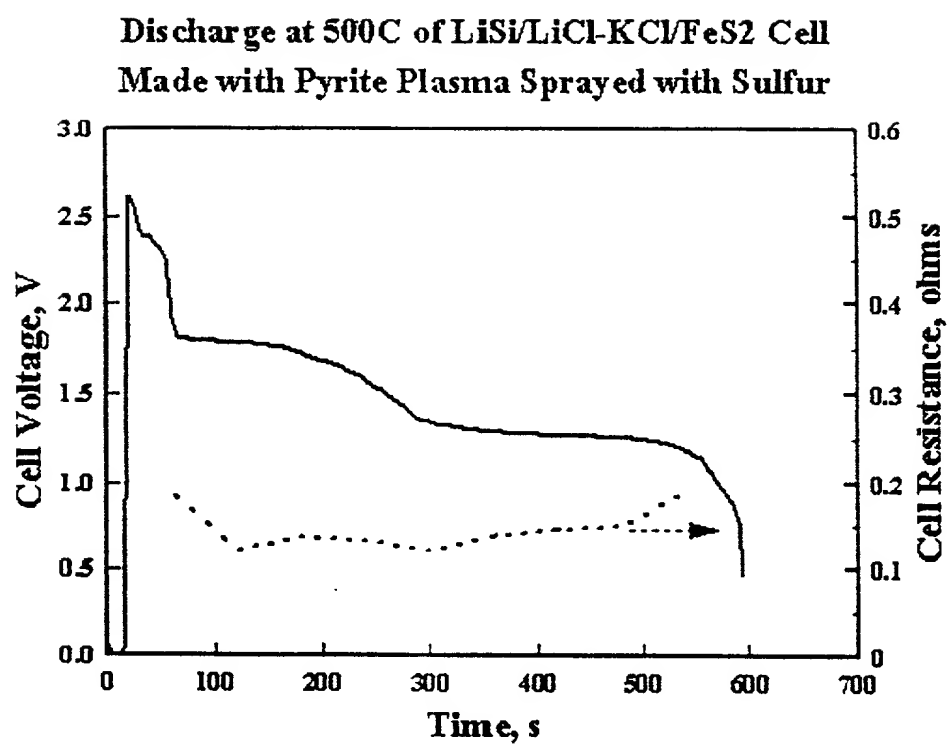


Figure 4. Discharge of Pyrite Plasma-Sprayed under Partial Pressure of Sulfur.

Discharge at 500C of LiSi/LiCl-KCl/FeS<sub>2</sub> Cell  
Made with Various Sources of Pyrite

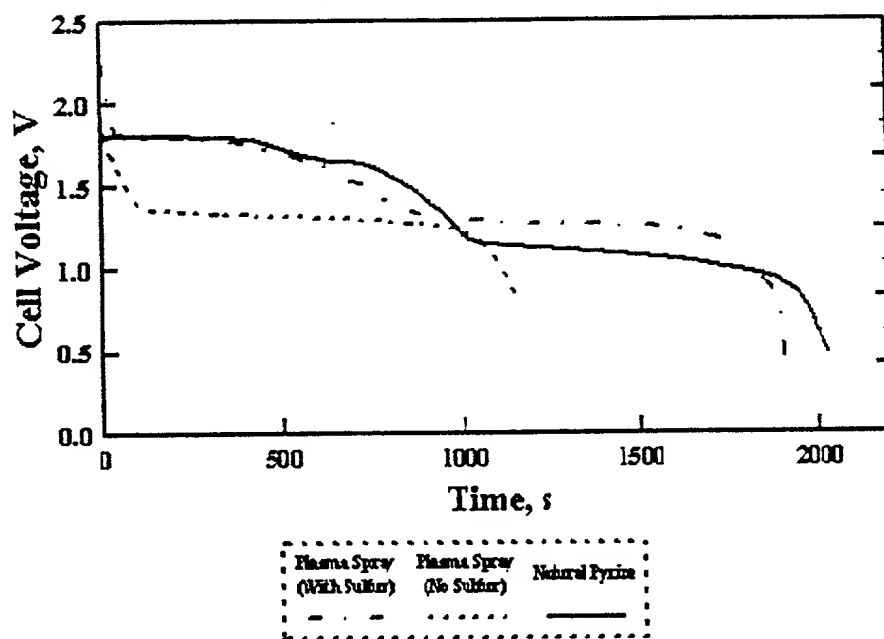


Figure 5.

### Resistance of LiSi/LiCl-KCl/FeS<sub>2</sub> Cells Discharged at 500C and Made with Various Pyrites

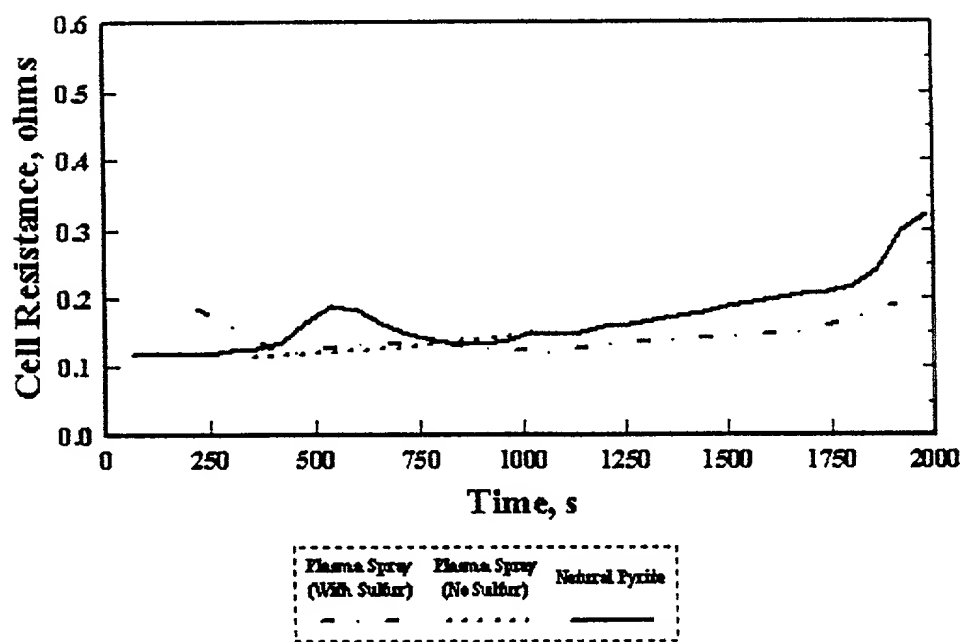


Figure 6.

# Combined Declaration for Patent Application and Power of Attorney

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name;

I believe that I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled

Energy Storage and Conversion Devices Using Thermal Sprayed Electrodes

the specification of which

(check one)

☒

is attached hereto.

☐ was filed on

as Application Serial No.

and (if applicable) was amended on:

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to the examination of this application in accordance with Title 37, Code of Federal Regulations, §1.56(a).

I hereby claim foreign priority benefits under Title 35, United States Code, §119 of any foreign application(s) for patent or inventor's certificate listed below and have also identified below any foreign application for patent or inventor's certificate having filing date before that of the application on which priority is claimed:

Prior Foreign Application(s)			Priority Claimed	
(Number)	(Country)	(Day Month Year Filed)	YES	NO

I hereby claim the benefit under Title 35, United States Code, §120 of any United States Application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulation, §1.56(a) which occurred between the filing date of the prior application and the national or PCT international filing date of this application:

(Application Serial No.)	(Filing Date)	(Status: patented, pending, abandoned)

I hereby claim the benefit under Title 35, United States Code, § 119(e) of any United States provisional application(s) listed below:

PROVISIONAL APPLICATION NUMBER

FILING DATE

60/106,681

November 2, 1998

I hereby appoint the following attorneys, with full power of substitution, association, and revocation, to prosecute this application and to transact all business in the Patent and Trademark Office connected herewith.

Michael A. Cantor	-	Registration No. 31,152
Philmore H. Colburn II	-	Registration No. 35,101
Keith J. Murphy	-	Registration No. 33,979
Leah M. Reimer	-	Registration No. 39,341
David A. Fox	-	Registration No. 38,807
Edward J. Ellis	-	Registration No. 40,389
Michael J. Rye	-	Registration No. 34,422
William J. Cass	-	Registration No. 41,659
Pamela J. Curbelo	-	Registration No. 34,676
Andrew Ryan	-	Registration No. 43,070
James F. McLaughlin	-	Registration No. 38,048
Gerow D. Brill	-	Registration No. 34,554
Robert J. Feltovic	-	Registration No. 27,710
Juan C. Villar	-	Registration No. 34,271
Herbert M. Bedingfield, Jr.	-	Registration No. 44,530
Timothy J. Olson	-	Registration No. 42,962
Steve Leavitt	-	Registration No. P45,318
Christopher Boehm	-	Registration No. 41,624
Michael Buchanan	-	Registration No. 44,571
George Lyman	-	Registration No. 44,884
George H. Libman	-	Registration No. 27,984

ADDRESS ALL CORRESPONDENCE TO:

**CANTOR COLBURN LLP**  
**88 Day Hill Road**  
**Windsor, CT 06095, USA**

DIRECT ALL TELEPHONE CALLS TO

**Michael A. Cantor**  
**Philmore H. Colburn II**  
**(860) 688-4470**  
**Facsimile (860) 688-7016**

I hereby further declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application of any patent issued thereon.



